# **Removal of Zirconium (Zr) from Aqueous Solution by Polymer Enhanced Ultrafiltration**

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# **ABSTRACT**

Although the world output of zirconium has been declining, increasing zirconium consumption cannot compete with this situation. For this reason, removal and recovery of zirconium become important. This work is focused on the removal of Zirconium (as  $ZrO_2^{2+}$ )  $)$ ions from an aqueous solution using polymer-enhanced ultrafiltration (PEUF) techniques with water-soluble Poly (sodium-p-styrene sulfonate, SSS) sorbent. The negatively charged sulfonic acid groups in the polymer interact with positively charged  $ZrO_2^{2+}$  cation thereby enabling the efficient removal of  $ZrO_2$ <sup>2+</sup>through ultrafiltration. The effect of polymer: zirconium mole ratio, initial solution pH, and the presence of interfering ions on the removal of zirconium was investigated. The obtained results demonstrated that  $ZrO_2^{2+}$  can be removed from the aqueous solution by the PEUF technique with more than 99% efficiency at  $pH \ge 2$ using polymer:  $Zr$  molar ratio of  $5:1$ . The presence of interfering ions did not affect the percent removal of  $ZrO_2^{2+}$ . .

*Keywords*: Polymer-enhanced ultrafiltration, Heavy metal removal, Ion Exchange, water treatment, Zirconium

# **1.0 INTRODUCTION**

Zirconium (Zr) is widely distributed in the earth's crust. It is a significant material for nuclear energy application due to its high transparency to neutrons. It is widely used in industry as secondary metal as it has outstanding chemical, thermal and optical properties [1–3]. "The recovery and purification of nuclear-grade zirconium from spent nuclear fuel cladding have been of great interest due to vast economic and environmental benefits, which result in ~\$40 million/year due to the high cost of nuclear-grade zirconium and nuclear waste disposal savings" [4].

Various separation techniques such as biosorption, adsorption, ion exchange, solvent extraction were applied for the removal and recovery of Zr from aqueous solutions or real samples [2,5–8].

The PEUF is a hybrid process that combines water-soluble polymers and ultrafiltration (UF) techniques. In PEUF, water-soluble polymers have a relatively high molecular weight cut off (MWCO) that allows the UF membrane to reject. Such polymers also have functional groups to bind ions/small molecules. In this process, unwanted ions/small molecules are first complexed by a polymer to increase their molecular weight with a size larger than the pores of the selected membrane that can be retained whereas permeate water is then purified from the unwanted molecules/ions [9–12].

So far, various metal ions were removed from water by PEUF. For example, Chen *et al*. [13] used the

PEUF system to remove  $Na^+$ ,  $K^+$ ,  $Li^+$ , ionic s  $H^+$ , Mg<sup>2+</sup>, Ca<sup>2+</sup>, Sr<sup>2+</sup>, Ba<sup>2+</sup>, Cu<sup>2+</sup>, Pb<sup>2+</sup>, tempera  $Co<sup>2+</sup>$ , and  $Ni<sup>2+</sup>$  from an aqueous the parameters solution by using the SSS a water soluble polymer. The selectivity sequence of cation affinity for PSS was found to be Zr was investigated.  $Ba^{2+} > Pb^{2+} > Sr^{2+} > Ca^{2+} > Cu^{2+} > Co^{2+}$  $> Ni^{2+} > Mg^{2+} > H^+ > K^+ > Na^+ > Li^+.$ .

The authors also concluded that the concentration of water-soluble polymer in the solution has an important effect on the removal rate and when it was adjusted to  $3 \text{ g/L}$ , the  $80\%$  Pb<sup>2+</sup> and 71% Cu<sup>2+</sup> removal were styrene sulf obtained. Hamhami *et al*. [14] studied the recovery of samarium  $(Sm<sup>3+</sup>)$  from aqueous solutions by poly(sodium 4‐styrene sulfonate) assisted Merck Biomax 10 kDa UF disc ultrafiltration. The removal of  $Sm^{3+}$ increased with the increment of polymer concentration in the solution. However further increment in polymer concentration led to a decrease in  $Sm^{3+}$ removal. The authors stated that such decrement caused by several phenomena such as concentration polarization, membrane fouling, osmotic pressure, and precipitation. The solution pH was also affected the  $Sm^{3+}$  removal rate. At pH 1, about were stirred in U 10% Sm<sup>3+</sup> removed. When the pH of Zr ion-exchange reac the solution was increased to 6, removal of  $\text{Sm}^{3+}$  reached 94%. com

Rivas and Moreno-Villoslada [15] studied the removal of  $Cd^{2+}$  from an ultrat aqueous solution in the presence of Na<sup>+</sup> ion by PEUF using SSS water- tubes) in soluble polymer. In the absence of Na the complete removal of  $Cd<sup>2+</sup>$ achieved. perm In the presence of  $0.4$  M NaNO<sub>3</sub> removal of  $Cd^{2+}$  decreased.

However, to the best of our knowledge, the removal of Zr by PEUF has not been reported. This work aims to investigate the optimum conditions for the removal of Zr by PEUF. In the PEUF procedure, polymer dose (i.e. polymer: target element ratio), initial solution pH,

ionic , Pb 2+ , temperature, and applied pressure are strength (interfering ion), the parameters that affect the removal rate [16]. For this purpose, the effect of rpolymer: Zr ratio, initial solution pH, and interfering ions on the removal of

# **2.0 METHODS**

# **2.1 Materials**

removal were styrene sulfonate, SSS) with average ) from Across. Zirconyl chloride octahydrate The water-soluble Poly (sodium-p- MWCO 70 kDa was obtained from was obtained from Sigma-Aldrich. membrane was used in the experiments. The Amicon UFSC40001 dead-end stirred cell (400 mL capacity) was used in the experiments. The pH of the solutions was adjusted by using HCl or NH<sub>3</sub> solutions.

# **2.2 PEUF Procedure**

from an ultrafiltration test. The 100 mL + concentration of zirconium in the The 250 mL of zirconium containing (5 mg/L) solution and SSS polymer were stirred in UF cell for the polymer- Zr ion-exchange reaction. After 60 minutes, the cell pressurized by using compressed nitrogen gas with an operating pressure of 1 bar to start the permeate was collected (10 mL x 10 tubes) in permeate probes. The permeate was measured. The schematic diagram of the process is shown in Figure 1.



**Figure 1** Scheme of the polymer enhanced ultrafiltration, PEUF

The zirconium removal conditions were optimized by changing the PEUF parameters; polymer: Zr mole ratio (1:1, 5:1, 10:1), initial solution pH (1- 4), and presence of interfering ions (Na<sup>+</sup>, K<sup>+</sup>, Ca<sup>2+,</sup> and Mg<sup>2+</sup>) were  $\begin{array}{ccc} 90 \end{array}$   $\begin{array}{ccc} \text{M} & \text{M} \end{array}$ optimized.

The Zr removal, R, (i.e. rejection)<br>calculated as shown in Equation 1. was calculated as shown in Equation 1.

$$
R = \frac{c_0 - c_p}{c_0} * 100 \dots \dots \dots (1)
$$

where C<sub>o</sub> and C<sub>p</sub> are concentrations of  $60 + 60 + 60$  $ZrO_2^{2+}$  ions in the feed and permeate solutions, respectively.

#### **2.3 Characterization of SSS**

Fourier transform infrared (FT‐IR) measurements (KBr discs) were Truspec Micro recorded in the region of 4000–400 cm−1 on PerkinElmer spectrophotometer.

#### **2.4 Analyses**

The Alizarin Red S method [17] was used to determine the concentration of  $ZrO_2^{2+}$  by UV/VIS spectrophotometer added to (Agilent, Cary). The pH of the solution

was measured by a pH meter (FG2 model, Mettler-Toledo).

#### **3.0 RESULTS AND DISCUSSION**

# **3.1 Fourier Transform Infrared Spectroscopy (FTIR)**

Figure 2 displays the FTIR peaks of the polymer used in this experiment. The significant peak at  $3434$  cm<sup>-1</sup> is is related to intermolecular hydrogen bonding. The peak at around 2922 cm−1 is the C–H vibration. The peaks at  $1600 - 1400$  cm<sup>-1</sup> are attributed to aromatic ring C-H in-plane bending. The main characteristic band of SSS at 1038 and 1008 cm<sup>-1</sup> (due to  $\sim$  SO<sub>3</sub>Na group) [18–21].



**Figure 2** FTIR spectra of SSS

The elemental analysis of polymer was carried out by the Leco CHNS analyser. Results showed that the polymer consists of 35 % carbon, 3.6 % hydrogen and 9.2% sulphur.

### **3.2 Effect of Polymer: Zr Mole Ratio on the Removal**

The various dose of the polymer was added to Zr containing solutions (5 mg-Zr/L, pH 4) before filtration and in Figure 3. 100 Removal of  $Zr(96)$ 80 60 40 20

the resulting removal rate is depicted

**Figure 3** Removal of Zr as a function of polymer: Zr ratio

 $5:1$ 

Polymer: Zr ratio

 $10<sup>1</sup>$ 

As can be seen from the Figure the percent removal of Zr increased with an increment on polymer dose. This finding was coincident with the results of Barakat and Schmidt [9] and Sánchez *et al*. [22]. They also observed that increment in polymer: metal ion ratio improved the removal rate.

The increasing the polymer: Zr ratio allows more available ion exchange sites and in turn increases the removal efficiency. The ion-exchange reaction between the polymer and Zr is shown in Equation 2.

 $2R - SO_3^- Na^+ + ZrO_2^{2+} \leftrightarrows (R -$  found  $SO_3^-$ )<sub>2</sub> $ZrO_2^{2+}$  + 2 $Na^+$  … ... (2) at p

The optimum polymer: Zr dose was found to be 5:1 and such ratio was used in the further experiment.

#### **3.3 Effect of Initial Solution pH on the Removal**

In this series of experiment, initial solution pH varied from 1 to 4 while Zr concentration  $(5 \text{ mg-Zr/L})$  and polymer: Zr ratio was adjusted to 5:1. The removal rate of Zr versus different solution pH is depicted in Figure 4. It is clear from the figure that at  $pH_1$ , the SSS polymer could not remove the Zr. When the pH of the solution was increased, the percent removal of Zr increased also.



**Figure 4** Removal of Zr as a function of initial solution pH

This behaviour can be explained that there is a competition between  $H^+$ and  $ZrO_2^{2+}$  ions for the available functional groups of SSS. At pH 1, the concentration of  $H^+$  is larger than  $Zr$ and this leads to an increase in the ion exchange reaction rate of  $H<sup>+</sup>$  and leads to a low removal rate for Zr [21]. The optimum pH range was found as  $\geq 2$ .

 $2^2 \leq (R - 6)$  found that removal of Cu<sup>2+</sup> was 64.7% Similar results have been found in the literature for heavy metal removal using SSS polymer. Chen *et al*. [13] applied PEUF for  $Cu^{2+}$  removal. They at pH 2.2 and it was increased to 96.6 at pH 7. A much the same trend was observed for the removal of  $Sm^{3+}$  ion [14].

# **3.3 Effect of Interfering Ionson the Removal**

The interferences of ions were determined at pH 4 with polymer: Zr ratio 5:1. The concentration of Zr was adjusted as 5 mg/L and obtained results summarized in Table 1.

 $\theta$ 

 $1:1$ 

**Table 1** Effect of interfering ions on the removal of Zr



It is clear from Table 1 that; the Lucidum: removal rate was not affected at a low concentration of interfering ions.

Similar findings were reported by<br>Note at al. [23] They stated that at [3] Verbych *et al*. [23]. They stated that at low concentration of Na<sup>+</sup> and Ca<sup>2+</sup> in  $\frac{20}{3}$ the solution removal of  $Cu^{2+}$  was  $\qquad \qquad$ almost constant, when the  $Na<sup>+</sup>$  and  $M$  $Ca^{2+}$  in the solution 400 times higher than the  $Cu^{2+}$  concentration, the  $[4]$  R. removal rate of  $Cu^{2+}$  decreased.

Lam *et al*. [24] investigated the effect of  $Na^+$  on  $Ni^{2+}$  removal. The Zircal authors concluded that the presence of  $2x10^{-1}$  M Na<sup>+</sup>, Ni<sup>2+</sup> removal tended Nucl. Teq towards zero.

# **4.0 CONCLUSION**

The water-soluble SSS polymer was tested for the removal of Zr with PEUF. The optimum conditions for the  $Zr$ <br>removal were found as polymer  $Zr$ : [6] removal were found as polymer Zr: ratio 5:1 and pH  $\geq$ 2. The presence of interfering ions at low concentrations did not affect the removal rate.

In a conclusion, PEUF may be an alternative method for the removal of Zr from solutions.

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